## Lecture 6

## ENERGY LOSSES IN HYDRAULIC SYSTEMS

## Learning Objectives

Upon completion of this chapter, the student should be able to:

- State the differences between laminar and turbulent flows.
- Define Reynolds number and state its importance.
- Explain the Darcy-Weisbach equation.
- Explain the various types of joints used in fluid power.
- Evaluate the head losses for laminar and turbulent flow.
- Explain the various types of losses in fittings and valves.
- Design a system considering all head losses in the system.


### 1.1 Introduction

Liquids such as water or petrol flow much easily than other liquids such as oil. The resistance to flow is essentially a measure of the viscosity of a fluid. The greater the viscosity of a fluid, the less readily it flows and the more is the energy required to move it. This energy is lost because it is dissipated as heat.

Energy losses occur in valves and fittings. Various types of fittings, such as bends, couplings, tees, elbows, filters, strainers, etc., are used in hydraulic systems. The nature of path through the valves and fittings determines the amount of energy losses. The more circuitous is the path, the greater are the losses. In many fluid power applications, energy losses due to flow in valves and fittings exceed those due to flow in pipes. Therefore, a proper selection of fitting is essential. In general, the smaller the size of pipe and fittings, the greater the losses.

The resistance to flow of pipes, valves and fittings can be determined using empirical formulas that have been developed by experimentation. The energy equation and the continuity equation can be used to perform a complete analysis of a fluid power system. This includes calculating the pressure drops, flow rates and power losses for all components of the fluid power system.

The purpose of this chapter is to study the detailed circuit analysis of energy losses in fluid power systems containing valves, fittings and other power transmission and energy conversion elements.

### 1.2 Laminar and Turbulent Flows

When speaking of fluid flow, one refers to the flow of an ideal fluid. Such a fluid is presumed to have no viscosity. This is an idealized situation that does not exist. When referring to the flow of a real fluid, the effects of viscosity are introduced into the problem. This results in the development of shear stresses between neighboring fluid particles when they move at different velocities. In the case of an ideal fluid flowing in a straight conduit, all the particles move in parallel lines with equal velocity. In the flow of a real fluid, the velocity adjacent to the wall is zero; it increases rapidly within a short distance from the wall and produces a velocity profile such as shown in Figure1.1.


Figure 1.1 Typical velocity profile: (a) Ideal fluid.(b) Real fluid
There are two types of flow in pipes:

1. Laminar flow:This is also known as streamline or viscous flow and is illustrated in Fig.1.2. In streamline flow, the fluid appears to move by sliding of laminations of infinitesimal thickness relative to adjacent layers; that is, the particles move in definite and observable paths or streamlines. The flow characteristic of a viscous fluid is one in which viscosity plays a significant part.


Figure 1.2 Laminar flow
2.Turbulent flow: It is illustrated in Fig.1.3. It is characterized by a fluid flowing in random way. The movement of particles fluctuates up and down in a direction perpendicular as well as parallel to the mean flow direction.
This mixing action generates turbulence due to the colliding fluid particles. This causes a considerable more resistance to flow and thus greater energy losses than those produced by laminar flow. A distinguishing characteristic of turbulence is its irregularity, there being no definite frequency, as in wave motion, and no observable pattern, as in the case of large eddies.


Figure 1.3 Turbulent flow

### 1.3 Reynolds Number

In the flow of a fluid through a completely filled conduit, gravity does not affect the flow pattern. It is also obvious that capillarity is of no practical importance, and hence significant forces are inertial force and fluid friction due to viscosity. The same is true for an airplane traveling at speed below that at which compressibility of air is appreciable. Also, for a submarine submerged far enough so as not to produce waves on the surfaces, the only forces involved are those of friction and inertia.

Considering the ratio of inertial forces to viscous forces, the parameter obtained is called the Reynolds number, in honor of Osborne Reynolds, who presented this in a publication of his experimental work in 1882. He conducted a series of experiments to determine the conditions governing the transition from laminar flow to turbulent flow. Reynolds came to a significant conclusion that the nature of the flow depends on the dimensionless parameter, that is,

$$
\operatorname{Re}=\frac{v D \rho}{\mu}
$$

Where $v$ is the fluid velocity, $D$ is the inside diameter of the pipe, $\rho$ is the fluid density and $\mu$ is the absolute viscosity of the fluid.

1. If Reis less than 2000 , the flow is laminar.
2. If Reis greater than 4000 , the flow is turbulent.
3. Reynolds number between 2000 and 4000 covers a critical zone between laminar and turbulent flow.

It is not possible to predict the type of flow that exists within a critical zone. Thus, if the Reynolds number lies in the critical zone, turbulent flow should be assumed. If turbulent flow is allowed to exist, higher fluid temperatures occur due to greater frictional energy losses. Therefore, turbulent flow systems suffering from excessive fluid temperature can be helped by increasing the pipe diameter to establish laminar flow.

## Example 1.1

The kinematic viscosity of a hydraulic fluid is $0.0001 \mathrm{~m}^{2} / \mathrm{s}$. If it is flowing in a $30-\mathrm{mm}$ diameter pipe at a velocity of $6 \mathrm{~m} / \mathrm{s}$, what is the Reynolds number? Is the flow laminar or turbulent?

Solution: From the definition of Reynolds number, we can write

$$
\operatorname{Re}=\frac{v D \rho}{\mu}=\frac{v D}{\mu / \rho}=\frac{v D}{v}=\frac{6 \times 0.03}{0.0001}=1800 \text { <COMP: v and nu both being used> }
$$

SinceRe is less than 2000, the flow is laminar.

### 1.4 Darcy-Weisbach Equation

If a fluid flows through a length of pipe and pressure is measured at two stations along the pipe, one finds that the pressure decreases in the direction of flow. This pressure decrease is mainly due to the friction of the fluid against the pipe wall. Friction is the main cause of energy losses in fluid power systems. The prediction of this friction loss is one of the important problems in fluid power. It is a very complicated problem and only in special cases, the friction factor is computed analytically.

Head losses ina long pipe in which the velocity distribution has become fully established or uniform along its length can be found by Darcy's equation as

$$
H_{\mathrm{L}}=f\left(\frac{L}{D}\right)\left(\frac{v^{2}}{2 g}\right)
$$

wherefis the Darcy friction factor, $L$ is the length of pipe (m), $D$ is the inside diameter of the pipe $(\mathrm{m}), v$ is the average velocity $(\mathrm{m} / \mathrm{s})$ and $g$ is the acceleration of gravity $\left(\mathrm{m} / \mathrm{s}^{2}\right)$.

Theactual dependence of $f$ on $R_{e}$ has to be determined experimentally. It should be apparent that friction factors determined do not apply near the entrance portion of a pipe where the flow changes fairly quickly from one cross-section to the next or to any other flow in which acceleration terms are not negligible.

### 1.5 Frictional Losses in Laminar Flow

Darcy's equation can be used to find head losses in pipes experiencing laminar flow by noting that for laminar flow, the friction factor equals the constant 64 divided by the Reynolds number:

$$
f=\frac{64}{\mathrm{Re}}
$$

Substituting this into Darcy's equation gives the Hagen-Poiseuille equation:

$$
H_{\mathrm{L}}=\frac{64}{\operatorname{Re}}\left(\frac{L}{D}\right)\left(\frac{v^{2}}{2 g}\right)
$$

## Example 1.2

The kinematic viscosity of a hydraulic fluid is $0.0001 \mathrm{~m}^{2} / \mathrm{s}$. If it is flowing in a $20-\mathrm{mm}$ diameter commercial steel pipe, find the friction factor in each case:
(a) The velocity is $2 \mathrm{~m} / \mathrm{s}$.
(b) The velocity is $10 \mathrm{~m} / \mathrm{s}$.

## Solution:

a) If the velocity is $2 \mathrm{~m} / \mathrm{s}$, then

$$
\operatorname{Re}=\frac{v D \rho}{\mu}=\frac{v D}{\mu / \rho}=\frac{v D}{v}=\frac{2 \times 0.02}{0.0001}=400
$$

The flow is laminar. Now

$$
f=\frac{64}{\operatorname{Re}}=\frac{64}{400}=0.16
$$

(b) If the velocity is $10 \mathrm{~m} / \mathrm{s}$, then

$$
\operatorname{Re}=\frac{v D \rho}{\mu}=\frac{v D}{\mu / \rho}=\frac{v D}{v}=\frac{10 \times 0.02}{0.0001}=2000
$$

Theflow is laminar. Now

$$
f=\frac{64}{\operatorname{Re}}=\frac{64}{2000}=0.032
$$

## Example 1.3

The kinematic viscosity of a hydraulic fluid is $0.0001 \mathrm{~m}^{2} / \mathrm{s}$. If it is flowing in a $30-\mathrm{mm}$ diameter pipe at a velocity of $6 \mathrm{~m} / \mathrm{s}$, find the head loss due to friction in units of bars for a $100-\mathrm{m}$ smooth pipe. The oil has a specific gravity of 0.90 .

Solution: We have

$$
\operatorname{Re}=\frac{v D \rho}{\mu}=\frac{v D}{\mu / \rho}=\frac{v D}{v}=\frac{6 \times 0.03}{0.0001}=1800
$$

We can express the head loss in bar as

$$
\begin{aligned}
H_{\mathrm{L}} & =\frac{64}{\operatorname{Re}}\left(\frac{L}{D}\right)\left(\frac{v^{2}}{2 g}\right) \\
& =\frac{64}{1800}\left(\frac{100}{0.030}\right)\left(\frac{6^{2}}{2 \times 9.81}\right) \\
& =217.5 \mathrm{~m}
\end{aligned}
$$

Hence,

$$
\begin{aligned}
\Delta p & =\gamma H_{\mathrm{L}} \\
& =1000 \mathrm{~kg} / \mathrm{m}^{3} \times 0.90 \times 9.81 \mathrm{~m} / \mathrm{s}^{2} \times 217.5 \\
& =1.92 \mathrm{MN} / \mathrm{m}^{2} \\
& =1.92 \mathrm{MPa} \\
& =19.2 \mathrm{bar}
\end{aligned}
$$

### 1.6 Frictional Losses in Turbulent Flow

Darcy's equation can be used to find head losses in pipes experiencing turbulent flow. However, the friction factor in turbulent flow is a function of Reynolds number and the relative roughness of the pipe.

### 1.6.1 Effect of Pipe Roughness

The relative roughness of pipe is defined as the ratio of inside surface roughness ( $\varepsilon$ ) tothediameter:

$$
\text { Relative roughness }=\frac{\varepsilon}{D}
$$

Table 1.1 gives typical values of absolute roughness for various types of pipes.
Table 1.1Typical values of absolute roughness for various types of pipe

| Type of Pipe | $\varepsilon(\mathbf{m m})$ |
| :--- | :--- |
| Glass or plastic | Smooth |
| Drawn tube | 0.0015 |
| Wrought iron | 0.046 |
| Commercial steel | 0.046 |
| Asphalted cast iron | 0.12 |
| Galvanized iron | 0.15 |
| Cast iron | 0.26 |
| Riveted steel | 1.8 |

To determine the values of the friction factor for use in Darcy's equation, we use the Moody diagram. If we know the relative roughness and Reynolds number, the friction factor can be determined easily. No curves are drawn in the critical zone, Re lies in between 2000 and 4000because it is not possible to predict whether flow is laminar or turbulent in this region. At the left end of the chart (Reynolds number less than 2000), the straight line curves give the relationship for laminar flow:

$$
f=\frac{64}{\mathrm{Re}}
$$

### 1.7 Frictional Losses in Valves and Fittings

For many fluid power applications, the majority of the energy losses occur in valves and fittings in which there is a change in the cross-section of flow path and a change in the direction of the flow. Tests have shown that head losses in valves and fittings are proportional to the square of the velocity of the fluid:

$$
H_{\mathrm{L}}=K\left(\frac{v^{2}}{2 g}\right)
$$

Where $K$ is called the loss coefficient of valve or fittings. $K$ factors for commonly used valves are given in Table1.2.

Table 1.2 $K$ factors for commonly used valves

| Valve or Fitting |  | $\boldsymbol{K}$ Factor |
| :--- | :--- | :--- |
| Globe valve | Wide open | 10 |
|  | 1/2 open | 12.5 |
| Gate valve | Wide open | 0.20 |
|  | $3 / 4$ open | 0.90 |
|  | $1 / 2$ open | 4.5 |
|  | $1 / 4$ open | 24 |
| Return bend | 2.2 |  |
| Standard tee | 1.8 |  |
| Standard elbow | 0.90 |  |
| $45^{\circ}$ elbow | 0.42 |  |
| $90^{\circ}$ elbow | 0.75 |  |
| Ball check valve | 4 |  |
| Union socket | 0.04 |  |

### 1.8 Equivalent Length Technique

We can find a length of pipe that for the same flow rate would produce the same head loss as a valve or fitting. This length of pipe, which is called the equivalent length of a valve or fitting, can be found by equating head losses across the valve or fitting and the pipe:

$$
K\left(\frac{v^{2}}{2 g}\right)=f\left(\frac{L}{D}\right)\left(\frac{v^{2}}{2 g}\right)
$$

Thisgives

$$
L_{\mathrm{e}}=\left(\frac{K D}{f}\right)
$$

where $L_{\mathrm{e}}$ is the equivalent length of a valve or fitting.

## Example 1.4

For the hydraulic system shown in the Fig. 1.4, the following data are given:
(a) A pump adds 2.984 kW to a fluid (pump hydraulic power $=2.984 \mathrm{~kW}$ ).
(b) The elevation difference between stations 1 and 2 is 6.096 m .
(c) The pump flow rate is $0.00158 \mathrm{~m}^{3} / \mathrm{s}$.
(d) The specific gravity of oil is 0.9 .
(e) The kinematic viscosity of oil is 75 cS .
(f) The pipe diameter is 19.05 mm .
(g) Pipe lengths are as follows: $0.305,1.22$ and 4.88 m .

Find the pressure available at the inlet to the hydraulic motor. The pressure at the oil top surface level in the hydraulic tank is atmospheric (0 Pa gauge).


Figure 1.4

## Solution:

Kinematic viscosity $=75 \mathrm{cS}=75 \times 10^{-6} \mathrm{~m}^{2} / \mathrm{s}$
We write the energy equation between stations 1 and 2:

$$
Z_{1}+\frac{p_{1}}{\gamma}+\frac{v_{1}^{2}}{2 g}+H_{\mathrm{p}}-H_{\mathrm{m}}-H_{\mathrm{L}}=Z_{2}+\frac{p_{2}}{\gamma}+\frac{v_{2}^{2}}{2 g}
$$

Since there is no hydraulic motor between stations 1 and 2,

$$
H_{\mathrm{m}}=0, v_{1}=0 \text { and } \frac{P_{1}}{\gamma}=0
$$

as oil tank is vented to the atmosphere. Now,

$$
Z_{2}-Z_{1}=6.096 \mathrm{~m}
$$

The velocity at point 2 is

$$
v_{2}=\frac{Q\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{A\left(\mathrm{~m}^{2}\right)}=\frac{0.00158}{\frac{\pi(0.01905)^{2}}{4}}=5.54 \mathrm{~m} / \mathrm{s}
$$

The velocity head at point 2 is

$$
\frac{v_{2}^{2}}{2 g}=\frac{5.54^{2}}{2 \times 9.81}=1.57 \mathrm{~m}
$$

Also,

$$
\operatorname{Re}=\frac{v D \rho}{\mu}=\frac{v D}{\mu / \rho}=\frac{v D}{v}=\frac{5.54 \times 0.01905}{75 \times 10^{-6}} \cong 1400
$$

So the flow is laminar. The friction is

$$
f=\frac{64}{\operatorname{Re}}=\frac{64}{1400}=0.0457
$$

We can now find the head loss due to friction between stations 1 and 2 :

$$
H_{\mathrm{L}}=\frac{f L_{\mathrm{p}}}{D_{\mathrm{p}}} \times \frac{v^{2}}{2 g}
$$

where
and

$$
\begin{aligned}
L_{\mathrm{p}} & =4.88+0.305+1.22+\left(\frac{K D}{f}\right)_{\text {std elbow }} \\
& =6.41+\left(\frac{0.9 \times 0.01905}{0.4057}\right) \\
& =6.79 \mathrm{~m} \\
H_{\mathrm{L}} & =\frac{0.0457 \times 6.79}{0.01905} \times 1.57=25.6 \mathrm{~m}
\end{aligned}
$$

Next use Bernoulli's equation to solve for $P_{2} / \gamma$ :

$$
\begin{aligned}
Z_{1}+\frac{p_{1}}{\gamma} & +\frac{v_{1}^{2}}{2 g}+H_{\mathrm{p}}-H_{\mathrm{m}}-H_{\mathrm{L}}=Z_{2}+\frac{p_{2}}{\gamma}+\frac{v_{2}^{2}}{2 g} \\
& \Rightarrow \frac{p_{2}}{\gamma}=\left(Z_{1}-Z_{2}\right)+H_{\mathrm{p}}+\frac{p_{1}}{\gamma}-\frac{v_{2}^{2}}{2 g}-H_{\mathrm{L}} \\
& =-6.096+H_{\mathrm{p}}+0-25.6-1.57 \\
& =H_{\mathrm{p}}-33.2
\end{aligned}
$$

The pump head is given by

$$
H_{\mathrm{P}}=\frac{P(\mathrm{~W})}{\gamma\left(\mathrm{N} / \mathrm{m}^{3}\right) \times Q\left(\mathrm{~m}^{3} / \mathrm{s}\right)}
$$

Now $\gamma=8817 \mathrm{~N} / \mathrm{m}^{3}$ and $P=2984 \mathrm{~W}$. So

$$
H_{\mathrm{P}}=\frac{2984 \mathrm{~W}}{8817\left(\mathrm{~N} / \mathrm{m}^{3}\right) \times 0.00158\left(\mathrm{~m}^{3} / \mathrm{s}\right)}=214.3 \mathrm{~m}
$$

Now

$$
\begin{aligned}
\frac{p_{2}}{\gamma} & =H_{\mathrm{p}}-33.2 \\
& =214.3-33.2 \\
& =181.1 \mathrm{~m} \text { of oil }
\end{aligned}
$$

Finally, we solve for the pressure at station 2:

$$
\frac{p_{2}}{\gamma}=181.1 \times 8817=1600000=1600 \mathrm{kPa}
$$

## Example 1.5

The oil tank for a hydraulic system (shown in Fig. 1.5) has the following details:
(a) The oil tank is air pressurized at 68.97 kPa gauge pressure.
(b) The inlet to the pump is 3.048 m below the oil level.
(c) The pump flow rate is $0.001896 \mathrm{~m}^{3} / \mathrm{s}$.
(d) The specific gravity of oil is 0.9 .
(e) The kinematic viscosity of oil is 100 cS .
(f) Assume that the pressure drop across the strainer is 6.897 kPa .
(g) The pipe diameter is 38.1 mm .
(h) The total length of the pipe is 6.097 m .

Find the pressure at station 2.


Figure 1.5
Solution: Givenp1 $=68.97 \mathrm{kPa}, \mathrm{Z} 1-\mathrm{Z2}=3 \mathrm{~m}, \mathrm{Q}=0.001896 \mathrm{~m} 3 / \mathrm{s}, \mathrm{ps}=6.897 \mathrm{kPa}, \mathrm{SG}=0.9, \mathrm{Dp}=$ $38.1 \mathrm{~mm}, v=100 \mathrm{cS}=100 \times 10-6 \mathrm{~m} 2 / \mathrm{s}, \mathrm{Lp}=6 \mathrm{~m}$. We have to find P 2 . This problem can be solved by the application ofmodified Bernoulli's (energy) equation:

$$
Z_{1}+\frac{p_{1}}{\gamma}+\frac{v_{1}^{2}}{2 g}+H_{\mathrm{p}}-H_{\mathrm{m}}-H_{\mathrm{L}}=Z_{2}+\frac{p_{2}}{\gamma}+\frac{v_{2}^{2}}{2 g}
$$

Also, given

$$
Z_{1}-Z_{2}=3 \mathrm{~m}
$$

We can write $H_{\mathrm{m}}=0$, as there being no motor between points1 and 2, the motor head is zero. Assuming the oil tank area (cross-section) to be large, the velocity at point 1 is $v_{1}=0$ (negligible velocity). To solve for $P_{2}$, let us compute and substitute different quantities into the energy equation.
The pressure head at station 1 is

$$
\frac{p_{1}}{\gamma}=\frac{68970}{8817}=7.82 \mathrm{~m}
$$

The velocity at point 2 is

$$
v_{2}=\frac{Q\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{A\left(\mathrm{~m}^{2}\right)}=\frac{0.001896}{\frac{\pi\left(0.0381^{2}\right)}{4}}=1.66 \mathrm{~m} / \mathrm{s}
$$

The velocity head at point 2 is

$$
\begin{aligned}
& \frac{v_{2}^{2}}{2 g}=\frac{1.66^{2}}{2 \times 9.81}=0.141 \mathrm{~m} \text { The Reynolds number is } \\
& \operatorname{Re}=\frac{v D \rho}{\mu}=\frac{v D}{\mu / \rho}=\frac{v D}{v}=\frac{1.66 \times 0.0381}{100 \times 10^{-6}} \cong 632
\end{aligned}
$$

So the flow is laminar. The friction is

$$
f=\frac{64}{\operatorname{Re}}=\frac{64}{632}=0.101
$$

Point 2 is before the pump; therefore, $H_{\mathrm{p}}=0$.
We can now find the head loss due to friction between stations 1 and 2

$$
H_{\mathrm{L}}=\frac{f L_{\mathrm{p}}}{D_{\mathrm{p}}} \times \frac{v^{2}}{2 g}+\text { Head loss across the strainer }
$$

Three standard elbows are used:

$$
\begin{aligned}
L_{\mathrm{p}} & =6.097+3\left(\frac{K D}{f}\right)_{\text {std elbow }} \\
& =6.097+3\left(\frac{0.9 \times 0.0381}{0.101}\right)=7.12
\end{aligned}
$$

Pressure drop across the strainer is 6.9 kPa . The head loss across strainer can be calculated as

$$
\text { Head loss across strainer }=\frac{\Delta p_{\text {strainer }}}{\gamma}=\frac{6900}{8817}=0.782 \mathrm{~m}
$$

Now use Bernoulli's theorem

$$
\begin{gathered}
Z_{1}+\frac{p_{1}}{\gamma}+\frac{v_{1}^{2}}{2 g}+H_{\mathrm{p}}-H_{\mathrm{m}}-H_{\mathrm{L}}=Z_{2}+\frac{p_{2}}{\gamma}+\frac{v_{2}^{2}}{2 g} \\
\Rightarrow \frac{p_{2}}{\gamma}=\left(Z_{1}-Z_{2}\right)+\frac{p_{1}}{\gamma}-H_{\mathrm{L}}-\frac{v_{2}^{2}}{2 g} \\
\Rightarrow \frac{p_{2}}{\gamma}=3.048+7.82-3.44-0.141 \\
=7.29 \mathrm{~m} \text { of oil }
\end{gathered}
$$

Finally, we solve for $p_{2}$ :

So

$$
\begin{gathered}
\frac{p_{2}}{\gamma}=7.29 \\
p_{2}=7.29 \times 8817=64300 \mathrm{~Pa}=64.3 \mathrm{kPa}
\end{gathered}
$$

If point 2 is after the pump, the pump head is given by

$$
H_{\mathrm{p}}=\frac{P(\mathrm{~W})}{\gamma\left(\mathrm{N} / \mathrm{m}^{3}\right) \times Q\left(\mathrm{~m}^{3} / \mathrm{s}\right)}
$$

Here $\gamma=8817 \mathrm{~N} / \mathrm{m}^{3}$. We know that

$$
\begin{gathered}
\operatorname{Power}(P)=p_{1} \times Q \\
\Rightarrow P=68.97\left(\mathrm{kN} / \mathrm{m}^{3}\right) \times 0.001896\left(\mathrm{~m}^{3} / \mathrm{s}\right)=0.13 \mathrm{~kW}
\end{gathered}
$$

So, pump head is

$$
H_{\mathrm{p}}=\frac{0.13 \times 10^{3} \mathrm{~W}}{8817\left(\mathrm{~N} / \mathrm{m}^{3}\right) \times 0.001896\left(\mathrm{~m}^{3} / \mathrm{s}\right)}=7.7 \mathrm{~m}
$$

We also know that

$$
\begin{gathered}
Z_{1}+\frac{p_{1}}{\gamma}+\frac{v_{1}^{2}}{2 g}+H_{\mathrm{p}}-H_{\mathrm{m}}-H_{\mathrm{L}}=Z_{2}+\frac{p_{2}}{\gamma}+\frac{v_{2}^{2}}{2 g} \\
\Rightarrow \frac{p_{2}}{\gamma}=\left(Z_{1}-Z_{2}\right)+\frac{p_{1}}{\gamma}-H_{\mathrm{L}}+H_{\mathrm{p}}-\frac{v_{2}^{2}}{2 g} \\
\Rightarrow \frac{p_{2}}{\gamma}=3.048+7.82-3.44+7.7-0.141 \cong 15 \mathrm{~m} \text { of oil }
\end{gathered}
$$

Finally, we solve for $p_{2}$ :

$$
\begin{gathered}
\frac{p_{2}}{\gamma} \cong 15 \\
\Rightarrow p_{2}=15 \times 8817=132255 \mathrm{~Pa}=132.26 \mathrm{kPa}
\end{gathered}
$$

## Example 1.7

For the system shown in Fig. 1.6, the following new data are applicable:
Pipe 1: length $=8 \mathrm{~m}, \mathrm{ID}=25 \mathrm{~mm}$
Pipe 2: length $=8 \mathrm{~m}, \mathrm{ID}=25 \mathrm{~mm}$
The globe valve is 25 mm in size and is wide open.
$\mathrm{SG}=0.90$ kinematic viscosity $\left(v=0.0001 \mathrm{~m}^{2} / \mathrm{s}\right)$ and $Q=0.0025 \mathrm{~m}^{3} / \mathrm{s}$
Find $p_{2}-p_{1}$ in units of bars.


Figure 1.6

Solution: The velocity can be calculated as

$$
v=\frac{Q\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{A\left(\mathrm{~m}^{2}\right)}=\frac{0.0025}{\frac{\pi\left(0.025^{2}\right)}{4}}=5.09 \mathrm{~m} / \mathrm{s}
$$

We know that

$$
\operatorname{Re}=\frac{v D \rho}{\mu}=\frac{v D}{\mu / \rho}=\frac{v D}{v}=\frac{5.09 \times 0.025}{0.0001} \cong 1272
$$

So the flow is laminar. Now friction factor is

$$
f=\frac{64}{\operatorname{Re}}=\frac{64}{1272}=0.0503
$$

Also, head loss is

$$
H_{\mathrm{L}}=\frac{f L_{\mathrm{p}}}{D_{\mathrm{p}}} \times \frac{v^{2}}{2 g}
$$

Now

$$
L_{\mathrm{p}}=8+8+\left(\frac{K D}{f}\right)_{\text {std elbow }}=16+\left(\frac{10 \times 0.025}{0.0503}\right)=21 \mathrm{~m}
$$

$K=10$ for globe valve (fully open). So

$$
H_{\mathrm{L}}=\frac{0.0503 \times 21}{0.025} \times \frac{5.09^{2}}{2 \times 9.81}=55.8 \mathrm{~m} \text { of oil }
$$

Now

$$
\begin{aligned}
& \frac{\Delta p}{\gamma}=H_{\mathrm{L}} \\
& \Rightarrow \Delta p=\gamma H_{\mathrm{L}} \\
&=(1000 \times 0.9 \times 9.81) \times 55.8 \\
&=493000 \mathrm{~N} / \mathrm{m}^{2}
\end{aligned}
$$

So

$$
\begin{aligned}
p_{2}-p_{1} & =-\Delta p \\
& =493000 \mathrm{~N} / \mathrm{m}^{2} \\
& =-493 \mathrm{kPa}=-4.93 \mathrm{bar}
\end{aligned}
$$

## Example 1.8

For the system shown in Fig. 1.7, the following data are applicable: $P_{1}=7 \mathrm{bar}, Q=0.002 \mathrm{~m}^{3} / \mathrm{s}$.
Pipe: total length $=15 \mathrm{~m}$ and $\mathrm{ID}=38 \mathrm{~mm}$
Oil: $\mathrm{SG}=0.90$ and kinematic viscosity $\left(\nu=0.0001 \mathrm{~m}^{2} / \mathrm{s}\right)$
Solve for $p_{2}$ in units of bars.


Pipe length $=\mathbf{4} \mathbf{m}$
Pipe length $=\mathbf{6 m}$

Figure 1.7

Solution: The velocity $V$ is

$$
v=\frac{Q\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{A\left(\mathrm{~m}^{2}\right)}=\frac{0.002}{\frac{\pi(0.038)^{2}}{4}}=1.76 \mathrm{~m} / \mathrm{s}
$$

We know that

$$
\operatorname{Re}=\frac{v D \rho}{\mu}=\frac{v D}{\mu / \rho}=\frac{v D}{v}=\frac{1.76 \times 0.038}{0.0001} \cong 669
$$

So the flow is laminar. The friction is

$$
f=\frac{64}{\operatorname{Re}}=\frac{64}{669}=0.096
$$

Now we can calculate the equivalent length ( $L_{\mathrm{e}}$ ) as

$$
\begin{aligned}
L_{\mathrm{e}} & =L_{\text {pipe }}+\left(\frac{K D}{f}\right)_{\text {globe valve }}+2\left(\frac{K D}{f}\right)_{90} \text { elbow } \\
& =15+\left(\frac{10 \times 0.038}{0.096}\right)+2\left(\frac{0.75 \times 0.038}{0.096}\right) \\
& =15+4+0.6=19.6 \mathrm{~m}
\end{aligned}
$$

Head loss due to friction is given by

$$
H_{\mathrm{L}}=\frac{0.096 \times 19.6}{0.038} \times \frac{1.76^{2}}{2 \times 9.81}=7.82 \mathrm{~m} \text { of oil }
$$

Now we can express the head loss due to friction in terms as pressure using

$$
\begin{gathered}
\frac{\Delta p}{\gamma}=H_{\mathrm{L}} \\
\Rightarrow \Delta p=\gamma H_{\mathrm{L}}=(1000 \times 0.9 \times 9.81) \times 7.82 \\
=690000 \mathrm{~N} / \mathrm{m}^{2}=0.69 \mathrm{bar}
\end{gathered}
$$

From the pressure drop we can calculated $p_{2}$ as

$$
\begin{aligned}
& p_{1}-p_{2}=\Delta p=0.69 \mathrm{bar} \\
& \Rightarrow 7-p_{2}=0.69 \mathrm{bar} \\
& \quad \Rightarrow p_{2}=6.31 \mathrm{bar}
\end{aligned}
$$

## Example 1.9

For the fluid power system shown in Fig. 1.8, determine the external load $F$ that a hydraulic cylinder can sustain while moving in an extending direction. Take frictional pressure losses into account. The pump produces a pressure increase of 6.9 MPa from the inlet port to the discharge port and a flow rate of $0.00253 \mathrm{~m}^{3} / \mathrm{s}$. The following data are applicable.

| Kinematic viscosity | $0.0000930 \mathrm{~m}^{2} / \mathrm{s}$ |
| :--- | :--- |
| Weight density of oil | $7840 \mathrm{~N} / \mathrm{m}^{3}$ |
| Cylinder piston diameter | 0.203 m |
| Cylinder rod diameter | 0.102 m |

All elbows are at $90^{\circ}$ with $K$ factor $=0.75$. Pipe length and inside diameters are given in Fig. 1.7.


Figure 1.8

| Pipe Number | Length $(\mathbf{m})$ | Diameter | Pipe Number | Length (m) | Diameter |
| :--- | :--- | :--- | :--- | :--- | :--- |
| 1 | 0.610 | 0.0381 | 8 | 1.52 | 0.0254 |
| 2 | 1.83 | 0.0381 | 9 | 1.52 | 0.0190 |
| 3 | 0.610 | 0.0381 | 10 | 1.52 | 0.0190 |
| 4 | 15.2 | 0.0254 | 11 | 18.3 | 0.0190 |
| 5 | 3.05 | 0.0254 | 12 | 3.05 | 0.0190 |
| 6 | 1.52 | 0.0254 | 13 | 6.10 | 0.0190 |
| 7 | 1.52 | 0.0254 |  |  |  |

(a) Determine the heat generation rate.
(b) Determine the extending and retracting speeds of cylinder.

Solution: We can use the following equations

$$
H_{\mathrm{L}}=\sum_{1}^{13}\left(\frac{f L_{\mathrm{p}}}{D_{\mathrm{p}}}+K\right) \frac{v^{2}}{2 g}
$$

Now

$$
v=\frac{Q\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{A\left(\mathrm{~m}^{2}\right)}
$$

We know that
$\operatorname{Re}=\frac{v D \rho}{\mu}=\frac{v D}{\mu / \rho}=\frac{v D}{v}$
Also

$$
Q_{\text {reurn }}=0.00253 \times \frac{\left(0.203^{2}-0.102^{2}\right)}{0.203}=0.00189 \mathrm{~m}^{3} / \mathrm{s}
$$

Velocity calculation:

$$
\begin{aligned}
& v_{1,2,3}=\frac{0.00253\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{\frac{\pi\left(0.0381^{2}\right)}{4} \mathrm{~m}^{2}}=2.22 \mathrm{~m} / \mathrm{s} \\
& v_{4,5,6}=\frac{0.00253\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{\frac{\pi\left(0.0254^{2}\right)}{4} \mathrm{~m}^{2}}=4.99 \mathrm{~m} / \mathrm{s} \\
& v_{7,8}=\frac{0.00189\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{\frac{\pi\left(0.0254^{2}\right)}{4} \mathrm{~m}^{2}}=3.73 \mathrm{~m} / \mathrm{s} \\
& v_{9,10}=\frac{0.00253\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{\frac{\pi\left(0.0190^{2}\right)}{4} \mathrm{~m}^{2}}=8.92 \mathrm{~m} / \mathrm{s} \\
& v_{11,12,13}=\frac{\frac{0.00189\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{\frac{\pi\left(0.0190^{2}\right)}{4} \mathrm{~m}^{2}}=6.67 \mathrm{~m} / \mathrm{s}}{}
\end{aligned}
$$

Reynolds number calculation:

$$
\begin{aligned}
& \operatorname{Re}_{(1,2,3)}=\frac{2.22 \times 0.0381}{0.000093}=909 \\
& \operatorname{Re}_{(4,5,6)}=\frac{4.99 \times 0.0254}{0.000093}=1362 \\
& \operatorname{Re}_{(7,8)}=\frac{3.73 \times 0.0254}{0.000093}=1018 \\
& \operatorname{Re}_{(9,10)}=\frac{8.92 \times 0.019}{0.000093}=1822 \\
& \operatorname{Re}_{(1,12,13)}=\frac{6.67 \times 0.019}{0.000093}=1363
\end{aligned}
$$

All flows are laminar. Now

$$
f=\frac{64}{\mathrm{Re}}
$$

Now head loss can be calculated for each element:

$$
\begin{gathered}
H_{\mathrm{L}(1,2,3)}=\left(\frac{64}{909} \frac{3.05}{0.0381}+1.5\right) \frac{2.22^{2}}{2 \times 9.81}=1.79 \mathrm{~m}=14000 \mathrm{~Pa} \\
H_{\mathrm{L}(4,5,6)}=\left(\frac{64}{1362} \frac{19.8}{0.0254}+10.5\right) \frac{4.99^{2}}{2 \times 9.81}=59.8 \mathrm{~m}=469000 \mathrm{~Pa} \\
H_{\mathrm{L}(7,8)}=\left(\frac{64}{1018} \frac{3.05}{0.0254}+0.75\right) \frac{3.73^{2}}{2 \times 9.81}=5.89 \mathrm{~m}=46200 \mathrm{~Pa} \\
H_{\mathrm{L}(9,10)}=\left(\frac{64}{1822} \frac{3.05}{0.019}+0.75\right) \frac{8.92^{2}}{2 \times 9.81}=25.9 \mathrm{~m}=203000 \mathrm{~Pa} \\
H_{\mathrm{L}(11,12,13)}=\left(\frac{64}{1363} \frac{27.4}{0.019}+1.5\right) \frac{6.67^{2}}{2 \times 9.81}=157 \mathrm{~m}=1230000 \mathrm{~Pa}
\end{gathered}
$$

Nowexternal load $F$ that a hydraulic cylinder can sustain while moving in an extending directioncan be calculated as

$$
\begin{aligned}
& F=[\text { Pressure on piston side } \times \text { Area }]-[\text { Pressure on rod side } \times \text { Area }] \\
& F=\left[[(6900000)-(14000+469000+203000)] \times \frac{\pi\left(0.203^{2}\right)}{4}\right]-\left[(46200+1230000) \times \frac{\pi\left(0.203^{2}-0.102^{2}\right)}{4}\right] \\
& F=(201000)-(30900)=170000 \mathrm{~N}
\end{aligned}
$$

(a) Heat generation rate (power loss in watts) $=$ Pressure $\times$ Discharge

Power loss $=\{(14000+469000+20300) \times(0.00253)+(46200+1230000) \times(0.00189)\}$

$$
=1740+2410
$$

$$
=4150 \mathrm{~W}=4.15 \mathrm{~kW}
$$

(b) Now to calculate forward and retracting speed of the cylinder

$$
\text { Forward velocity of the piston }=\frac{Q_{\text {pump }}}{\text { Area of the piston }}
$$

$Q_{\text {pump }}=0.00253 \mathrm{~m}^{3} / \mathrm{s}$
Cylinder piston diameter $=0.2032 \mathrm{~m}$
Area of piston $A=\frac{\pi\left(0.2032^{2}\right)}{4} \mathrm{~m}^{2}$
Knowing the area of piston and discharge we can calculate the forward velocity of piston as

$$
V_{\text {extending }}=\frac{Q\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{A\left(\mathrm{~m}^{2}\right)}=\frac{0.00253}{\frac{\pi\left(0.2032^{2}\right)}{4}}=0.0780 \mathrm{~m} / \mathrm{s}
$$

Now

$$
\text { Return velocity of the piston }=\frac{Q_{\text {pump }}}{\text { Annulus area }}
$$

Cylinder rod diameter $=0.1016 \mathrm{~m}$
Area of $\operatorname{rod}=\frac{\pi\left(0.1016^{2}\right)}{4} \mathrm{~m}^{2}$
Annulus area $=\frac{\pi\left(0.2032^{2}\right)}{4}-\frac{\pi\left(0.1016^{2}\right)}{4}$
Knowing the annulus area and discharge we can calculate the return velocity of piston as

$$
V_{\text {extending }}=\frac{Q\left(\mathrm{~m}^{3} / \mathrm{s}\right)}{A\left(\mathrm{~m}^{2}\right)}=\frac{0.00253}{\frac{\pi\left(0.2032^{2}\right)}{4}-\frac{\pi\left(0.1016^{2}\right)}{4}}=0.104 \mathrm{~m} / \mathrm{s}
$$

## Objective-Type Questions Fill in the Blanks

1. In fluid power systems, energy losses due to flow in valves and fittings may $\qquad$ those due to flow in pipes.
2. Darcy's equation can be used to find head losses in pipes experiencing $\qquad$ flow.
3. In the case of an ideal fluid flowing in a straight conduit, all the particles move in parallel lines with equal $\qquad$ _.
4. The flow characteristic of a viscous fluid is one in which $\qquad$ plays a significant part.
5. Energy loss in turbulent flow is $\qquad$ than laminar flow.

## State True or False

1. Reynolds number is the ratio of viscous forces to inertial force.
2. In the flow of a fluid through a completely filled conduit, gravity affects the flow pattern.
3. Friction is the main cause of energy losses in fluid power systems.
4. In the flow of a real fluid, the velocity adjacent to the wall is maximum.
5. A distinguishing characteristic of turbulence is its irregularity, no definite and no observable pattern.

## Review Questions

1. Differentiate between laminar flow and turbulent flow.
2. List the main causes of turbulence in fluid flow.
3. Define Reynolds number and list its range for laminar and turbulent flows.
4. Briefly explain the method to calculate the equivalent length of a valve or fitting.
5. Define the relative roughness and $K$ factor of a valve or fitting.
6. Write an expression for pressure drop down a pipe in terms of friction factor.
7. What are the important conclusions of the Reynolds experiment?
8. Name two causes of turbulence in fluid flow.
9. What is meant by the equivalent length of a valve or fitting?
10. Why is it important to select properly the size of pipes, valves and fittings in hydraulic systems?

Answers
Fill inthe Blanks
1.Exceed
2.Turbulent
3.Velocity
4.Viscosity
5.Less

State True or False
1.False
2.False
3.True
4.False
5.True

